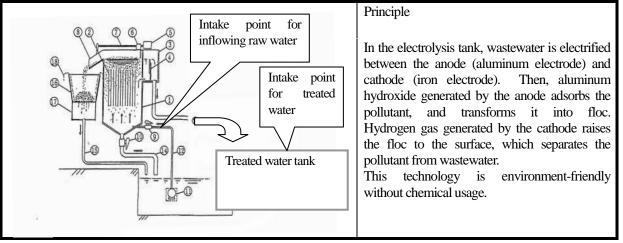


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O Overview	
Demonstration institution	Saitama-prefectural Environmental Analysis & Research Association
Period of the experiment for verification	From October 24, 2007 to January 31, 2008
Purpose of this technology	This technology includes a system that makes the oil in organic wastewater rise to the surface for collection by an electrolytic response. The system works as a unit that removes oil and as an auxiliary unit for grease interceptor that improves the quality of wastewater.

1. Outline of the technology intended for verification



2. Outline of the verification experiment

O Outline of the location for performing the verification experiment

Project type	Student's cafeteria (cafeteria #1, building #6 of Nippon Institute of Technology)					
Project scale	То	tal floor area: 1404.7 m	² Nu	mber of sea	ts: 1,000	
Address	4-1 Ga	kuen-dai Miyashiro-m	achi Minar	ni-saitama-	gun Saitam	a
Amount of wastewater during the verification experiment (L/min)	12L/min 5L/min 0 What was calculated treated at the experiment metering pump.	• $ + $ • $ + $ 2 4 in the verification exp ent location, but the ar				

O_Specifications and performance of the equipment used for verification

Category	Item	Specifications and performance		
Outline of	Model	DZ101KC		
the facility	Size and weight	$W = 770 \text{ mm} \times D = 1,300 \text{ mm} \times H = 1,300 \text{ mm} 100 \text{kg}$		
	Object	Normal-hexane extracts(<i>n</i> -Hex) biochemical oxygen demand(BOD)		
Design conditions	Amount of wastewater per day	Actual result: 7.5 m ³ /day (12 L/min setting) 2.9 m ³ /day (5 L/min setting)		
	Treatment object	<i>n</i> -Hex less than 30 mg/L (the original setting was more than 90% of removal rate for both <i>n</i> -Hex and BOD).		



3. Results of the verification experiment

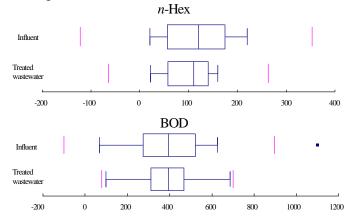
O Water q	uality verifi	ication items		
Items	Unit	Verification result (bottom line-top, median) upper: result of the research #1~#4* ² lower: result of the research for improvement and follow-up		
		Influent	Treated wastewater	Removal rate $(\%)^{*1}$
<i>n</i> -Hex	mg/L	20-220 (120) 24-110 (60)	22-160(110) 6-36 (20)	8.3-38.9 (25.7) 25-91.9 (66.7)
BOD	mg/L	66.4-625 (394) 167-463 (318)	99-685 (393) 122-337 (224)	<u>1.0-60.3 (23.2)</u> 7.5-38.5 (14.1)

*1. The removal rate was calculated according to the formula Rate=[(pollution loading amount of influent)-(pollution loading amount of treated wastewater)]/(pollution loading amount of influent)

*2. The results of the research #1~#4 indicates the water quality in the daily research, the weekly research, the regular research#1~#4.

(1)Result of the research $#1 \sim #4$

According to the result of the research $\#1 \sim \#4$, the removal rates for both *n*-Hex and BOD were low under the following operating conditions:(12L/min, voltage=5 V, current=20 A)

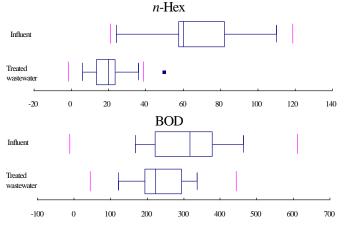


(2)Result of the research for improvement and follow-up

After the examination by the verification committee, the operating conditions were improved and the following results were obtained.

Improved specifications: The inflow was changed from 12 to 5 L/min, the voltage was changed from 5 to 8 V, and the current was changed from 20 to 40 A.

As a result of the improvement, the removal rate of n-Hex increased, and therefore, the quality of the wastewater met the quality standards (less than 30 mg/L). Moreover, the removal rate of BOD increased, although, this increase was not sufficient to make the wastewater quality meet the quality standards.





O Environmental impact items

5
Verification result
~3.7 kg/day as oily industrial wastes (content: 69.3%)
Nothing remarkable other than sludge
65 dB in treatment facilities,63 dB in neighboring areas
Odor index: less than 10

O Used resources index

Items	Verification result				
Amount of electric energy used	Electrolysis voltage: 5 V current: 20 A 0.14 W/L voltage: 8 V current: 40 A 1.07 W/L				
Amount of chemical used for wastewater treatment	No chemical was used				
Wastage of the aluminum sheet used as electrodes	The aluminum sheet (7.2 kg) to which a voltage of 5 V and a current of 20 A is applied should be changed every 450 h.(erosion 37.5% of the weight) The aluminum sheet (7.2 kg) to which a voltage of 8 V and a current of 40 A is applied should be changed every 130 h. (erosion 17.9% of the weight)				

O Operation and maintenance performance item

Maintenance items	Maintenance time per operation and maintenance frequency	Number of people and skill required for maintenance
Periodic check	60 min (twice a month)	One person having knowledge of operation and maintenance
Replacement of aluminum sheets	30 min (once every 600 h for electrolysis)	one person having knowledge of operation and maintenance

O Qualitative remark

Items	Remark			
	Although the desired water quality after the treatment could not be achieved the quality of the wastewater after <i>n</i> -Hex met the waste quality standards (less that 30 mg/L), as seen in the follow-up research after improvement(the average wa 22 mg/L.). In addition, it is expected that technical improvements such a batch-type operation might improve the removal performance.			
Remark on water quality	5L/min Batch expriment			
	Influent Treated Inflow 15 30 45 wastewater			
Time required for initiation	30 min(one person)			
Time required for shutdown	1 min			
Reliability of the equipment intended for verification	There was no trouble with the equipment intended for verification during the period of the verification experiment.			
How to solve the problems	The instruction manual is useful for solving problems.			
Evaluation of the instruction manual of operation and maintenance	There is nothing in particular to be improved.			
Others	Although the grease trap had been cleaned once a week normally, that was no cleaned during three months under the examination.			



(Reference information)

Note: The information on this page is what the environmental engineering developer applied on behalf of the technical bulletin on his own responsibility, and is an exception to the verification.

	Items		Description given by the	e environment	al-technology de	eveloper		
Name/type			Electrolytic wastewater treatment unit (DZ101KC)					
Manufacturer (distributor)			NT labo Co., Ltd.					
TEL/FAX Web address			TEL: (048)940	-2243 FAX:	(048)940-2246			
			http://www.nt - labo.co.jp					
COL	E-mail address		<u>in</u>	fo@nt-labo.co	<u>.jp</u>			
Si	ize and weight		$W=770 \text{ mm} \times D =$	1,300 mm×H	= 1,300 mm 100)kg		
pre	Necessity for e-treatment and post-treatment							
S	upplementary facility	sec	As for the treated wastewater and after-load raw water, the installation sedimentation tank or an overflow weir after treatment tank is require settling the suspended solids(SS).					
	of the equipment intended for verification		More than 10 years for vinyl chloride and steel work					
Tir	ne for initiation		30 min (performan	nce in the verifi	cation experime	nt)		
				Unit price	Quantity	Total		
		Ini	tial cost	• • • • • • • • •		2,200,000		
Approximate cost (yen) Data with the * mark are calculated from the result of the verification experiment			main body DZ101KC Installation costs(including trial operation)	2,000,000 150,000	1	2,000,000 150,000		
	-		Transportation cost	50,000	1	50,000		
	Rı	unning cost (monthly)			79,475			
	to with the * mark		a with the * mark		Electric power consumption cost	20 yen/kWh	580 kWh	11,600
	calculated from		Maintenance cost	30,000 yen/month	1	30,000		
		Waste disposal cost Waste transportation cost	25 yen/kg 25,000	215 kg (8.6 kg/day)	*5,375 *25,000			
	-		Other expenses(aluminum	yen/use 2,500	6 (used for	*7,500		
			sheet)	yen/sheet	two months)	,,000		

• Contrary to the aim of the verification experiment, the system could not treat the expected inflow sufficiently. However, after the improvement, the removal of *n*-Hex was affected.

- Low-priced electrodes are used for removal by electrolysis, which realizes high performance and low running cost.
- You can customize the size and the performance of the unit, depending on the circumstances.
- Once the unit is installed, you can operate it on the same day.